PATENT COOPERATION TREATY

PCT

| REC'D | 14 | JAN | 2005 |
|-------|----|-----|------|
| WIRO | | | POT |

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

(Chapter II of the Patent Cooperation Treaty)

(PCT Article 36 and Rule 70)

| Applicant's or agent's file reference SMR/P550634PC | FOR FURTHER ACT | ION s | See Form PCT/IPEA/416 | | | |
|---|--|--|--|--|--|--|
| International application No. | International filing date (da | y/month/year) | Priority date (day/month/year) | | | |
| PCT/GB2004/001123 17.03.2004 | | | 22.03.2003 | | | |
| International Patent Classification (IPC) or national classification and IPC | | | | | | |
| E21B43/34 | | | | | | |
| | | | | | | |
| | | | | | | |
| Applicant CALTEC LIMITED et al | | | | | | |
| OALI LO LIMIT LO GEGI | | | | | | |
| This report is the international pre Authority under Article 35 and trar | This report is the international preliminary examination report, established by this International Preliminary Examining Authority under Article 35 and transmitted to the applicant according to Article 36. | | | | | |
| 2. This REPORT consists of a total of | of 6 sheets, including this | cover sheet. | | | | |
| 3. This report is also accompanied b | | | | | | |
| a. 🛛 sent to the applicant and to | | | | | | |
| and/or sheets containi | sheets of the description, claims and/or drawings which have been amended and are the basis of this report and/or sheets containing rectifications authorized by this Authority (see Rule 70.16 and Section 607 of the Administrative Instructions). | | | | | |
| sheets which supersede earlier sheets, but which this Authority considers contain an amendment that goes beyond the disclosure in the international application as filed, as indicated in item 4 of Box No. I and the | | | | | | |
| Supplemental Box. | Turney and a total of find | icata tupo and numba | r of electronic carrier(s)) , containing a | | | |
| sequence listing and/or tal | nies related thereto, in cor | nputer readable torm | only, as indicated in the Supplemental | | | |
| Box Relating to Sequence | Listing (see Section 802 | of the Administrative I | Instructions). | | | |
| | | | | | | |
| | -lating to the following item | | | | | |
| 4. This report contains indications re | Hatting to the following ites | 115. | | | | |
| ☐ Box No. I Basis of the op | nion | | | | | |
| ☐ Box No. II Priority | | | | | | |
| | | i to novelty, inventive | step and industrial applicability | | | |
| ☐ Box No. IV Lack of unity of | | | | | | |
| Box No. V Reasoned state applicability; cit | ement under Article 35(2) tations and explanations s | with regard to novelty supporting such staten | r, inventive step or industrial nent | | | |
| ☐ Box No. VI Certain docume | ents cited | | | | | |
| ☐ Box No. VII Certain defects | in the international applic | ation | | | | |
| ☐ Box No. VIII Certain observe | ations on the international | application | | | | |
| | | | | | | |
| Date of submission of the demand | | Date of completion of th | is report | | | |
| 00.00.0004 | | 47.04.0005 | | | | |
| 29.09.2004 | | 17.01.2005 | | | | |
| Name and mailing address of the internation | nal | Authorized Officer | was Petanto. | | | |
| preliminary examining authority: | İ | | John Committee C | | | |
| European Patent Office - P.E NL-2280 HV Rijswijk - Pays | Bas | Dantinne, P | | | | |
| Tel. +31 70 340 - 2040 Tx: 3 Fax: +31 70 340 - 3016 | 1 651 epo nl | Telephone No. +31 70 | 340-3396 | | | |

٠:

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

International application No. PCT/GB2004/001123

| | Box No. I Basis of the report | | |
|--|---|---|--|
| 1. • | With regard to the language , this report is based on the international application in the language in which it was filed, unless otherwise indicated under this item. | | |
| | which is the language of a transitional search (und | stations from the original language into the following language , anslation furnished for the purposes of: er Rules 12.3 and 23.1(b)) tional application (under Rule 12.4) examination (under Rules 55.2 and/or 55.3) | |
| 2. | 2. With regard to the elements* of the international application, this report is based on (replacement sheets which have been furnished to the receiving Office in response to an invitation under Article 14 are referred to in this report as "originally filed" and are not annexed to this report): | | |
| | Description, Pages | | |
| | 1-10 | as originally filed | |
| Claims, Numbers 1-42 filed with telefax on 29.09.20 Drawings, Sheets | | | |
| | | filed with telefax on 29.09.2004 | |
| | | | |
| | 1/4-4/4 | as originally filed | |
| | a sequence listing and/or ar | ny related table(s) - see Supplemental Box Relating to Sequence Listing | |
| 3. | □ The amendments have rest □ the description, pages □ the claims, Nos. □ the drawings, sheets/figs □ the sequence listing (sp □ any table(s) related to se | S . | |
| 4. | had not been made, since they Supplemental Box (Rule 70.2(c | s pecify): pequence listing <i>(specify)</i> : | |
| | * If item 4 applies, s | ome or all of these sheets may be marked "superseded." | |

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

International application No. PCT/GB2004/001123

Box No. V Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

4. Statement

Novelty (N)

Yes: Claims

3-6,8,9,11,13-17,20,22,24,26,27,29,31,33-37,40,42

No: Claims

1,2,7,10,12,18,19,21,23,25,28,30,32,38,39,41

Inventive step (IS)

Yes: Claims

No: Claims

1 - 42

Industrial applicability (IA)

Yes: Claims

1 - 42

No: Claims

2. Citations and explanations (Rule 70.7):

see separate sheet

Re Item V

Reasoned statement with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

Reference is made to the following documents:

- D1: WO 95/07414 A (SARSHAR MIR MAHMOOD ;BHR GROUP LTD (GB)) 16 March 1995 cited in the application
- D2: GB-A-2 239 676 (BHR GROUP LTD) 10 July 1991
- D3: GB-A-2 014 862 (INST FRANCAIS DU PETROL) 5 September 1979
- D4: US-A-3 590 919 (TALLEY WILLIAM A JR) 6 July 1971
- D5: WO 02/18746 A (ABB RESEARCH LTD ;BRINGEDAL BJORN OEYVIND (NO); NOEKLEBERG LARS (N) 7 March 2002
- 1) The present application does not meet the criteria of Article 33(1) PCT, because the subject-matter of claim 1 is not new in the sense of Article 33(2) PCT.
- 1.1) The document **D1** discloses (the references in parentheses applying to this document; see fig.3; page 4 line 12 27):

A system for pumping multiphase fluids, the system including:

- a phase separator (42) that is connected to receive a LP multiphase fluid (11), and is constructed and arranged to separate a LP gas phase (42G) and a LP liquid phase (42L) from the LP multiphase fluid (11);
- a gas-gas jet pump (32) having a LP inlet connected to receive the LP gas phase (42G) from the phase separator (42), a HP inlet connected to receive a HP gas supply (41G) from a sustainable gas source, and an outlet for providing outlet gas (43G) at a pressure higher than that of the LP gas phase (42G);
- and a liquid pump (31) having a LP inlet connected to receive the LP liquid phase (42L) from the phase separator (42), and an outlet for providing outlet liquid (43) at a pressure higher than that of the LP liquid phase (42L).

D1 discloses the use of gas from a high pressure well as a sustainable gas source. HP wells have a wide range of pressure and a pressure range of 50-150 bar is considered

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY (SEPARATE SHEET)

PCT/GB2004/001123

an implicit feature of D1 (See guidelines C-IV- 7.2) The pressure required is obviously dependent of the LP pressure gas well which need to be boosted. The pressure required for the motive fluid will be determined by the man skilled in the art knowing the pressure of the well to be boosted. He will use whatever fluid is easily available and at low cost. This might be high pressure gas from high pressure wells or other sources available at the well site like gas lift, export gas or even simply the use of a compressor.

The subject-matter of claim 1 is therefore not new (Article 33(2) PCT).

- 2) The same reasoning applies, mutatis mutandis, to the subject-matter of the corresponding independent claim 23, which therefore is also considered not new.
- 3) Dependent claims 2-22 and 24-42 do not contain any features which, in combination with the features of any claim to which they refer, meet the requirements of the PCT in respect of novelty and/or inventive step for the following reasons:

Claims 2-4,24,25: As a drive medium for a jet pump, the man skilled in the art will use whatever fluid is easily available and low cost. Lift gas is well known to lift well fluid and is an obvious choice as a drive medium. Export gas is disclosed in D1 as it is gas from other HP wells. D2 discloses the use of a compressor (16') to use gas as a drive medium in a jet pump (17). Steam is often used in stimulation operations and is also an obvious option for the man skilled in the art.

Claims 5,6,13,14,20,22,26,27,29,33,34,40,42: The subject-matter of these claims consists in the selection of a range of pressure/ratio. Such a selection can only be regarded as inventive, if the range presents unexpected effects or properties in relation to the rest of the range. However, no such effects or properties are indicated in the application. Hence, no inventive step is present in the subject-matter of these claims. Claims 7-9,28: D3 discloses the use of a mechanical pump to pump the liquid. Also disclosed in D1 (fig.5; réf. 55). PDM is an obvious choice. D3 discloses similar outlet pressure for liquid and gas phases (page 1 line 52 - 70).

Claims 10-12,30-32: D1 discloses a liquid-liquid jet pump (41). HP liquid phase from HP wells is considered as a sustainable source. D5 (fig. 1 réf. 6) discloses the use of injection water as a drive medium to entrain another fluid. D1 also discloses the use of HP oil (41L) from other wells as drive medium.

Claims 15,16,35,36: D4 discloses a knock-out vessel for the same purpose.

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY (SEPARATE SHEET)

International application No.

PCT/GB2004/001123

Claims 17,37: a cyclone separator is usual in such process (see also cited documents in the application).

Claims 18,19,21,38,39,41: D1 and D3 discloses a mixing device (6) for combining gas and liquid phases. A commingler is an obvious choice. D3 is about producing multiphasic oil effluents.

CLAIMS

- 1. A system for pumping multiphase fluids, the system including:
 - a phase separator that is connected to receive a LP multiphase fluid, and is constructed and arranged to separate a LP gas phase and a LP liquid phase from the LP multiphase fluid;
 - a gas-gas jet pump having a LP inlet connected to receive the LP gas
 phase from the phase separator, a HP inlet connected to receive a HP gas
 supply from a sustainable gas source, and an outlet for providing outlet gas
 at a pressure higher than that of the LP gas phase;
 - and a liquid pump having a LP inlet connected to receive the LP liquid phase from the phase separator, and an outlet for providing outlet liquid at a pressure higher than that of the LP liquid phase;
 - wherein the sustainable gas source has a pressure in the range 50-150 bar.
- 2. A system according to claim 1, wherein the sustainable gas source comprises a supply of lift gas or export gas.
- A system according to claim 1, wherein the sustainable gas source comprises a supply of steam from geothermal wells.
- 4. A system according to any one of the preceding claims, wherein the sustainable gas source includes a compressor.
- A system according to any one of the preceding claims, wherein the HP gas supply has a pressure at least twice that of the LP gas phase.
- A system according to any one of the preceding claims, wherein the gas-gas jet pump has an outlet pressure in the range 1.1 to 3.0 times the pressure of the LP multiphase fluid.
- 7. A system according to any one of the preceding claims, wherein the liquid pump is a mechanical pump.

10/09/2004

- 8. A system according to claim 7, wherein the liquid pump is a positive displacement pump.
- 9. A system according to claim 7 or claim 8, wherein the liquid pump has an outlet pressure similar to that of the gas-gas jet pump.
- 10. A system according to any one of claims 1 to 6, wherein the liquid pump is a liquid-liquid jet pump having a LP inlet connected to receive the LP liquid phase from the phase separator, a HP inlet connected to receive a HP liquid supply from a sustainable liquid source, and an outlet for providing outlet liquid at a pressure higher than that of the LP liquid phase
- A system according to claim 10, wherein the sustainable liquid source comprises a supply of injection water.
- A system according to claim 10, wherein the sustainable liquid source comprises a supply of export oil.
- 13. A system according to any one of claims 10 to 12, wherein the sustainable liquid source has a pressure at least twice that of the LP liquid phase.
- 14. A system according to any one claims 10 to 13, wherein the liquid-liquid jet pump has an outlet pressure in the range 1.1 to 3.0 times that of the LP liquid phase.
- 15. A system according to any one of the preceding claims, including a knock-out vessel for removing retained liquid from the LP gas phase.
- 16. A system according to claim 15, wherein the knock-out vessel has a liquid outlet connected to deliver removed liquid to the liquid pump.
- 17. A system according to any one of the preceding claims, wherein the separator is a cyclone type separator.
- 18. A system according to any one of the preceding claims, including a mixing device connected to the outlets of the jet pump and the liquid pump, for combining the outlet gas and the outlet liquid and providing a combined multiphase outlet fluid at a pressure higher than that of the LP multiphase fluid
- A system according to claim 18, wherein the mixing device is a commingler.

- 20. A system according to claim 18 or claim 19, wherein the combined multiphase outlet fluid has an outlet pressure in the range 1.1 to 3.0 times that of the LP liquid phase.
- 21. A system according to any one of claims 18 to 20, wherein the multiphase fluid is a petroleum gas/oil mixture.
- 22. A system according to claim 21, wherein the gas/liquid ratio of the petroleum gas/oil mixture is in the range 9 to 49 at the operating pressure and temperature.
- 23. A process for pumping multiphase fluids, the process including:
 - separating a LP multiphase fluid into a LP gas phase and a LP liquid phase;
 - Increasing the pressure of the LP gas phase using a gas-gas jet pump, by supplying a HP gas supply from a sustainable gas source to a HP inlet of the jet pump and supplying the LP gas phase to a LP inlet of the jet pump;
 - and increasing the pressure of the LP liquid phase using a liquid pump.
 - wherein the sustainable gas source has a pressure in the range 50-150 bar.
- 24. A process according to claim 23, wherein the sustainable gas source comprises a supply of lift gas.
- 25. A process according to claim 23, wherein the sustainable gas source comprises a supply of export gas.
- -26.- A process according to any one of claims 23-25; wherein the sustainable gas source has a pressure at least twice that of the LP gas phase.
- 27. A process according to any one of claims 23-26, wherein the gas-gas jet pump has an outlet pressure in the range 1.1 to 3.0 times the pressure of the LP multiphase fluid.
- 28. A process according to any one of claims 23-27, wherein the liquid pump is a mechanical pump.

- 29. A process according to claim 28, wherein the liquid pump has an outlet pressure in the range 1.1 to 3.0 times the pressure of the LP multiphase fluid.
- 30. A process according to any one of claims 23 to 27, wherein the liquid pump is a liquid-liquid jet pump having a LP inlet connected to receive the LP liquid phase, and a HP inlet connected to receive a HP liquid supply from a sustainable liquid source.
- A process according to claim 30, wherein the sustainable liquid source comprises a supply of injection water.
- 32. A process according to claim 31, wherein the sustainable liquid source comprises a supply of export oil.
- 33. A process according to any one of claims 23-32, wherein the sustainable liquid source has a pressure at least twice that of the LP multiphase fluid.
- 34. A process according to any one of claims 23-33, wherein the liquid-liquid jet pump has an outlet pressure in the range 1.1 to 3.0 times that of the LP multiphase fluid.
- 35. A process according to any one of claims 23-34, in which retained liquid is removed from the LP gas phase using a knock-out vessel.
- 36. A process according to claim 35, wherein removed liquid is delivered to the liquid pump.
- 37. A process according to any one of claims 23-36, wherein the LP gas and liquid phases are separated in a cyclone type separator.
- 38. A process according to any one of claims 23-37, including mixing the increased pressure gas and liquid phases to provide a combined multiphase fluid at a pressure higher than that of the LP multiphase fluid
- 39. A process according to claim 38, wherein increased pressure gas and liquid phases are mixed in a commingler.
- 40. A process according to any one of claims 38-39, wherein the combined multiphase outlet fluid has an outlet pressure in the range 1.1 to 3.0 times that of the LP multiphase fluid.

- 41. A process according to any one of claims 38-40, wherein the multiphase fluid is a petroleum gas/oil mixture.
- 42. A process according to claim 41, wherein the gas/liquid ratio of the petroleum gas/oil mixture is in the range 9 to 49 at the operating pressure and temperatures.